



EFFECT OF OIL LEVEL ON HYDRAULIC SYSTEM PERFORMANCE

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ABSTRACT

Oil level in hydraulic reservoir has been varied to study its undesirable effect on oil temperature. The study shows that the initial air cushion volume as well as its fluctuations, affect the pressure inside; thus aeration, cavitation and heat and mass transfer would be influenced. These conditions play the main role in optimizing the oil level in the reservoirs.

Taking into consideration the other working conditions (discharges, temperatures, oil properties...etc.), it was found that both high and low oil level would increase the working oil temperature.

INTRODUCTION

Hydraulic equipments have recently become so influential in the design of industrial machinery, that without hydraulics automation known nowadays would have not been possible [1]. Hydraulic power systems consist mainly of pumps, motors, cylinders, control valves and accessories. The term "ACCESSORIES" actually leads to a false impression, when considering their importance in system performance and safety. One of the very basic accessories is the oil tank in open circuits. Oil tank has a number of functions that affect widely the hydraulic circuit performance, among which - this paper is concerned with its work as ; heat exchanger and air separator. To fulfill these functions the tank size is chosen (3 to 5) times the pump flow rate per minute, with (10 to 15 %) of its volume as an air cushion[1]. An air breather with suitable filter is usually provided to allow the

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oil level fluctuation in a dust-proof space.

In some engineering applications, severe fluctuations of oil level are observed. For such cases, oil temperature increases for both lower and higher oil level than prescribed. The objective of this paper is to investigate these effects.

EFFECT OF OIL LEVEL

Oil level in the tank has a direct impact on the pump suction conditions as it usually causes an increase in oil temperature. This may be explained by :

- Decreasing the thermal capacity of the system reservoir.
- Increasing the probability of cavitation in the pump suction side.
- Promoting the formation of free vortex near the suction pipe, that increases the air entrainment from the atmosphere.
- Increasing the dissolved air liberation in the pump suction, which affects the pump volumetric efficiency.
- Increasing leakage due to lower oil viscosity in effect of higher temperatures.
- In addition to that, lower oil level promotes the suction of solid deposits, thus deterioration of both the pump all-together with the system service life.

To explain the temperature increase as the oil level gets higher, one should investigate its effect on:

- The rate of heat generation (hydraulic losses) in the oil.
- The rate of heat dissipation from the tank (cooling effect).

BASIC EQUATION GOVERNING THE PRESSURE VARIATION INSIDE.

The difference between input and output powers of the hydraulic system represents the heat delivered to the oil (losses). This energy is dissipated to the surroundings through the elements of the system, (oil tank and heat exchanger if found). The pumping volumetric efficiency has a direct impact on the over-all system losses.

For certain operating conditions, the effect of oil level on heat

generation rate may be investigated by evaluating the air pressure fluctuations above the oil in the tank. This pressure fluctuation has shown considerable contribution as to heat generation and dissipation.

For the oil tank given in fig.1, the continuity equation applied on the oil inside the tank, when neglecting the compressibility effect gives:

$$Q_n = Q_o - Q_i = A_T \cdot \frac{dy}{dt} \quad (1)$$

While for air enclosed above the oil in the tank, it gives: [2]

$$Q_a = A_T \cdot \frac{dy}{dt} + \left(\frac{V_{ao} + A_T \cdot y}{B} \right) \cdot \frac{dp}{dt} \quad (2)$$

where : $Q_a = C_d \cdot A_n \sqrt{2(p_o - p) / \rho} \quad (3)$

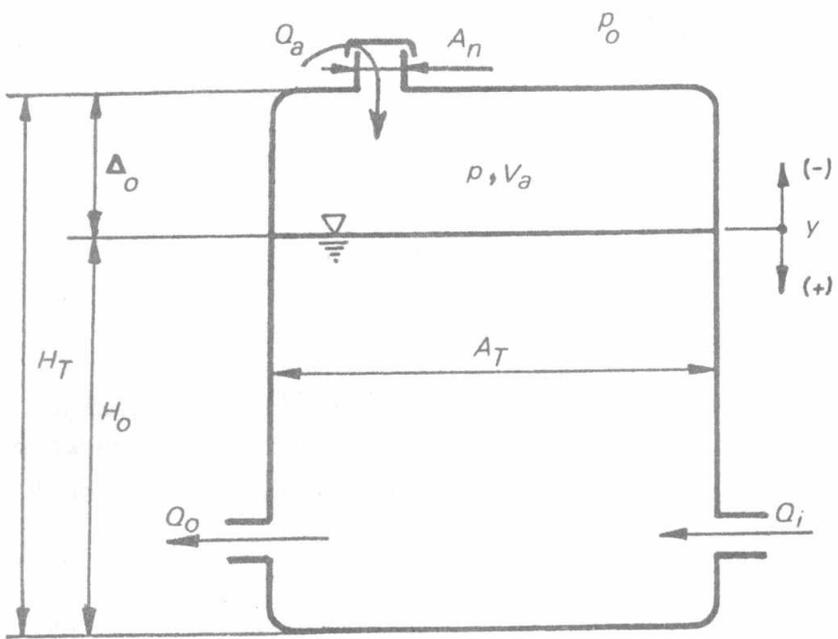


Fig.1. Basic parameters applied on the reservoir

* All the symbols are listed at the end of the paper.

From equations (1),(2) and (3):

$$C_d \cdot A_n \sqrt{\frac{2(p_o - p)}{\rho}} = Q_n + \frac{(V_{ao} + A_T \cdot y)}{n \cdot p} \cdot \frac{dp}{dt} \quad (4)$$

For specified flow conditions, and initial oil level, the differential equation (4) representing the air pressure p inside the tank can be solved numerically as function of time.

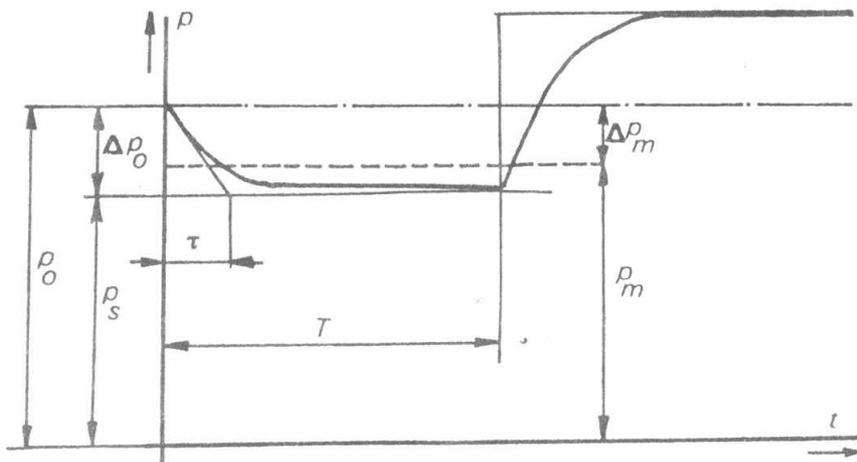


Fig.2. Time response of the reservoir system pressure

EFFECT OF THE INITIAL DEGREE OF FILLING OF OIL TANK [V_{ao} or H_o]

Basic differential equation (4) shows that according to the operating net flow rate Q_n of the oil, the pressure p inside the tank varies such that it approaches asymptotically the value p_s given by:

$$p_s = p_o - \frac{\rho \cdot Q_n^2}{2C_d^2 \cdot A_n^3} \quad (5)$$

with variable course of variation of time constant τ calculated as follows:

$$\frac{-\Delta p_o}{\tau} = \frac{dp}{dt}(0)$$

from which:
$$\tau = \frac{\rho \cdot V_{ao} \cdot Q_n}{2C_d^2 \cdot A_n^2 \cdot n \cdot p_o} \quad (6)$$

as:
$$V_{ao} = A_T \cdot \Delta_o = A_T \cdot (H_T - H_o)$$

the
$$\tau = \frac{\rho \cdot Q_n \cdot A_T (H_T - H_o)}{2C_d^2 \cdot A_n^2 \cdot n \cdot p_o} \quad (7)$$

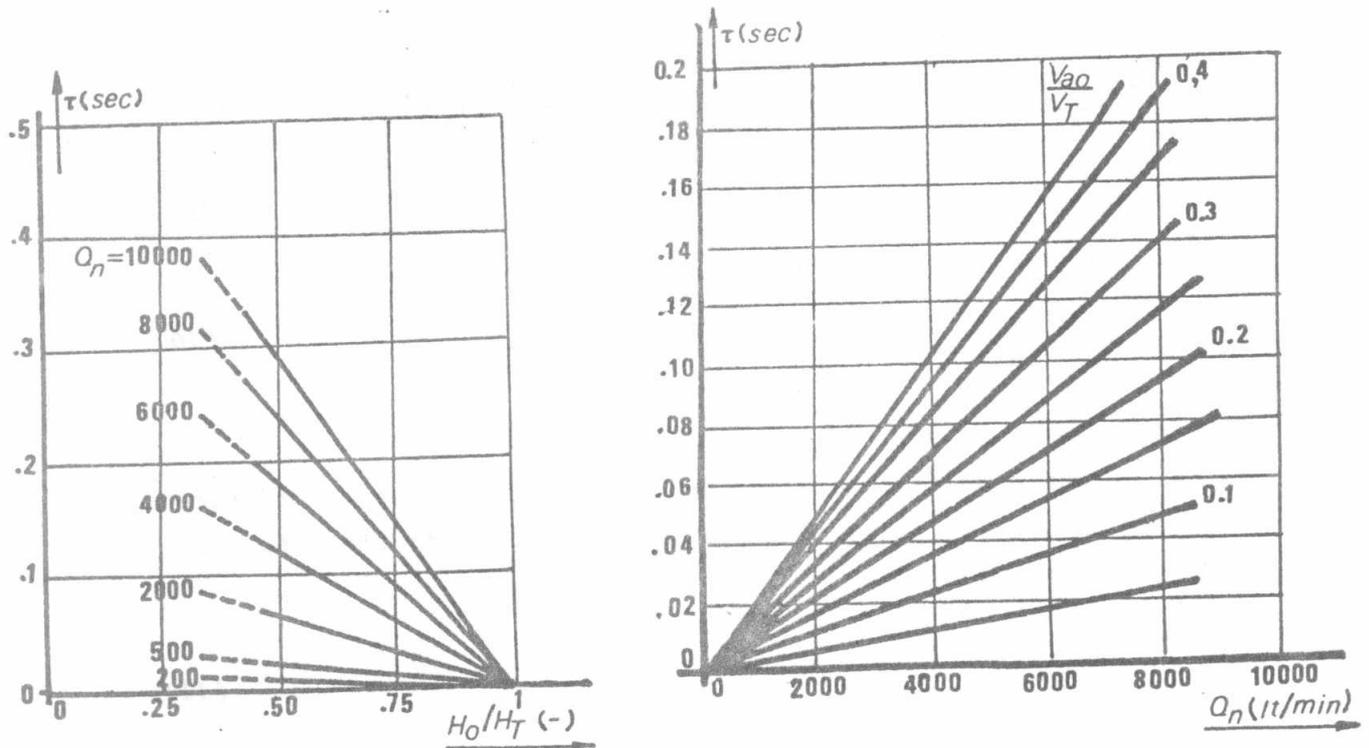


Fig.3. Effect of the degree of filling on the time constant

VOLUMETRIC EFFICIENCY DECREASE AND HEAT GENERATION

Reducing the pressure above the oil in the tank by Δp_m ; decreases the air solubility by $\Delta \epsilon_a$. [3]

$$\Delta \epsilon_a = -K \cdot \Delta p_m \quad (8)$$

where K is a constant depending on the oil.

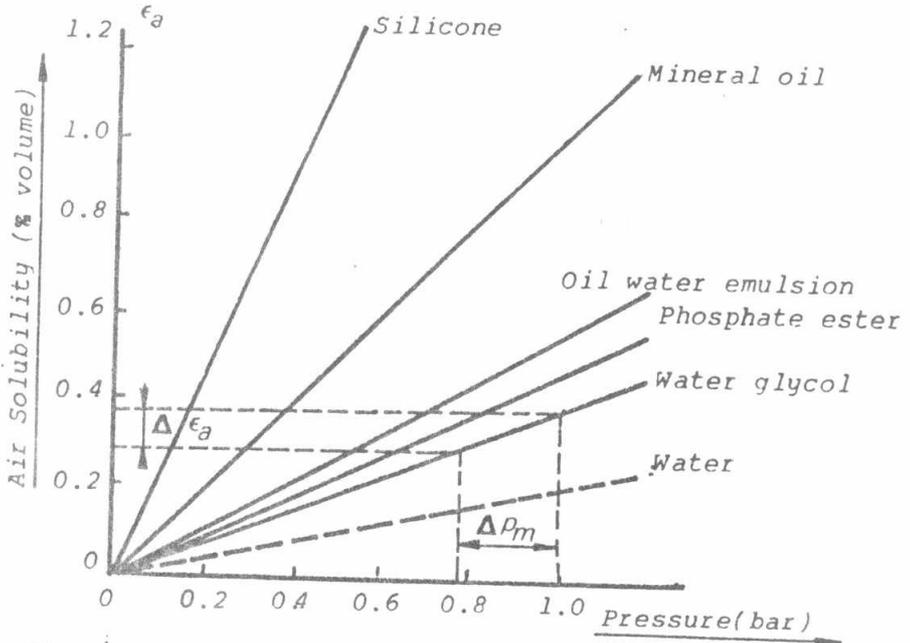


Fig.4. The solubility of air in various liquids

$$\Delta p_m = \Delta p_o \left(1 - \frac{\tau}{T_1} (1 - e^{-T_1/\tau}) \right) \tag{9}$$

where:

$$\Delta p_o = p_o - p_s = \frac{\rho Q_n^2}{2C_d^2 \cdot A_n^2} \tag{10}$$

For the vapour bubbles liberation during cavitation due to pressure drop, and by analogy, defining the ratio of its volume to the total oil by $\Delta \epsilon_v$, it may be assumed as:

$$\Delta \epsilon_v = -K_1 (p_m - p_{cr})^{n_1} \tag{11}$$

where K_1 and n_1 are to be found experimentally.

From equations (9) and (11), the total air and bubbles volumetric ratio to the working oil may be given by:

$$\Delta \epsilon_T = \Delta \epsilon_a + \Delta \epsilon_v \tag{12}$$

In this case, the volumetric efficiency η_{vo} will be reduced to : η_v given by:

$$\eta_v = \eta_{vo} (1 - \Delta \epsilon_T) \tag{13}$$

The rate of heat generation P_G will be increased by ΔP_G given by:

$$\Delta P_G = \left(\frac{\eta_{vo} - \eta_v}{\eta_{vo}} \right) P_{inp} = \Delta \epsilon_T \cdot P_{inp} \quad (14)$$

where:

$$P_G = (1 - \eta_o) P_{inp} \quad (15)$$

HEAT DISSIPATION FROM THE TANK

The heat transfer from the system reservoir takes place in two different ways:

- heat transfer through the tank walls.
- latent heat carried by oil vapour diffused in the air on top of the oil level.

Convection mode plays the major role in sensible heat transmission across the walls. On the other hand it is believed that thermal resistance of air film around the tank is predominant. In practice an overall heat transfer coefficient U ($5:20 \text{ W/m}^2 \cdot \text{C}^\circ$) is traced [4] and the sensible heat flux q_s is given by:

$$q_s = U \cdot \Delta T \quad (16)$$

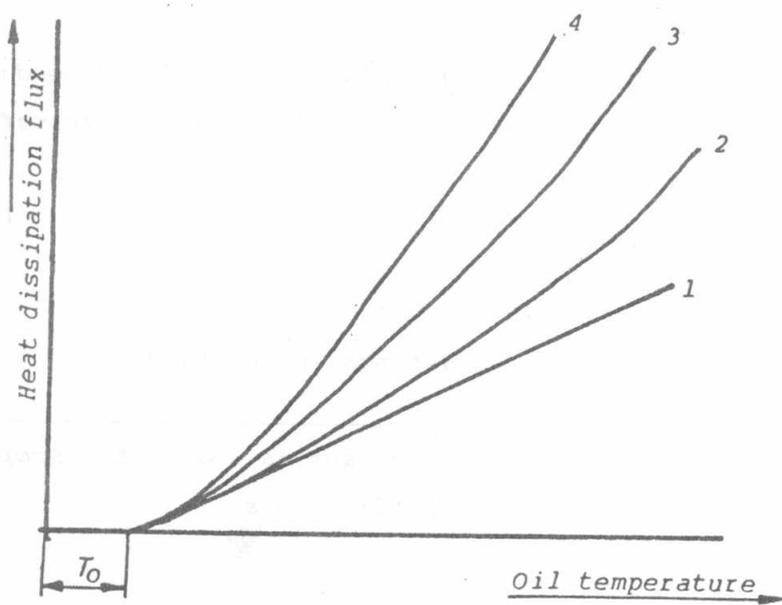


Fig.5. Typical heat dissipation flux

Line (1) in figure 5 represents that equation, and shows the dependence of q_s on the oil temperature.

The mass transfer within the oil tank enclosure depends on the regime of air motion inside. This regime will be handled in the first approximation as stagnant conditions with stationary oil level. Thus the mass flux of oil vapour across the area of interface is given by:

$$m'_o = -D \rho \frac{dw}{d\Delta_o} + w \rho v_s \quad [5] \quad (17)$$

Although air is assumed stagnant, its bulk will have certain velocity v_s [in last equation] away of the surface. This velocity is determined utilizing the stagnation condition.

Taking the fluctuations of the oil level into consideration, accounts for an increase of the velocity of the air bulk by v_c . This velocity has been estimated through a computer program based on the mathematical model representing the air motion due to the fluctuations of the oil level in the tank. Such effect showed some 100 times the effect of molecular diffusion. Finally a worked out formula of the total latent heat flux can be written as:

$$q_1 = C_1 \cdot \frac{A'}{A} \cdot \frac{D \cdot \rho}{\Delta_o} \cdot \frac{p_v}{p_m - p_v} \left[1 + \frac{\Delta_o}{2D} (v_s + v_c) \right] \cdot L_v \quad (18)$$

Further numerical approximation would probably be useful depending on the rough estimated value of v_c^* , and equation (18) may be simplified as:

$$q_1 = C_2 \cdot \frac{A'}{A} \cdot \rho \cdot \frac{p_v}{p_m - p_v} \cdot v_c \cdot L_v \quad (19)$$

The constant C_2 in the last equation depends on the type

* Detailed study of air motion inside the tank is beyond the scope of work and will be continued in later publications.

of used oil, and average oil concentration in the bulk of the air (between the two values of equilibrium concentration in the interface area, and zero oil concentration at the top of the tank). The ratio A'/A relates q_1 to the surface area of oil tank A Instead of the area of interface A' .

Equation 19 is then represented by the exponential form lines (2,3 &4) for different total air pressures $p_2 > p_3 > p_4$ shown in figure (5).

Illustrative case study was conducted on 50% ethylene waterglycol mix and results are shown in figure (6).

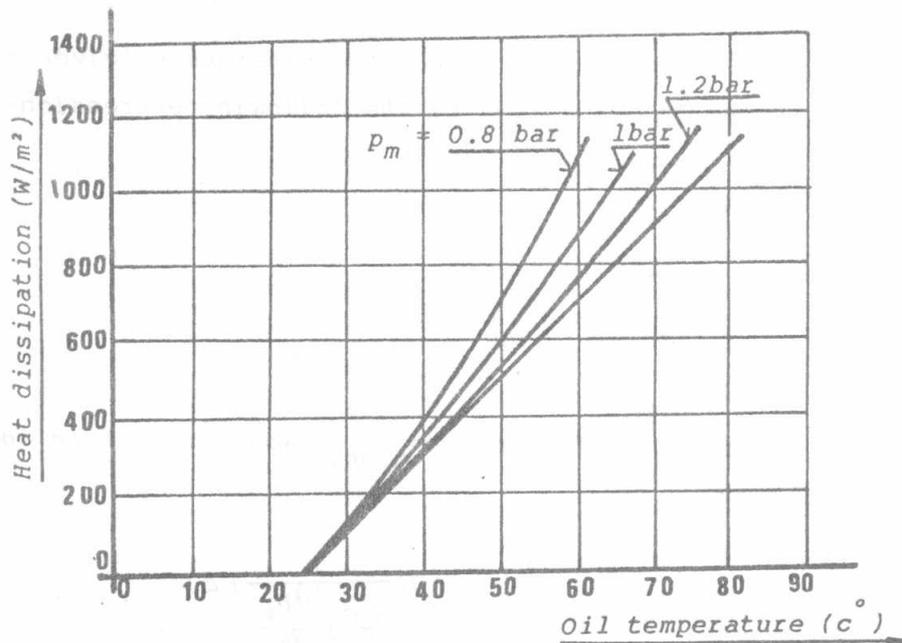


Fig.6. Heat dissipation determined for the case study

The fluctuations of oil level has an effect on the latent heat flux as follows: when the oil level drops down during active strokes, the total air pressure inside the tank is reduced as previously shown, thus accounting for higher equilibrium concentration of oil vapour into air, hence increased flux. On the other hand, oil level fluctuations increase the velocity of the air bulk which plays an important role in mass transfer.

It must be noticed that the type of oil (i.e vapour pressure characteristics) is the most significant factor in the whole process and for oils of low vapour pressure, the latent heat flux may be ignored, while for oils of high p_v (e.g waterglycols) such effect is appreciable.

DETERMINATION OF THE OPTIMUM DEGREE OF FILLING

For the steady state conditions and from equations (14) and (19):

$$\Delta \epsilon_T \cdot P_{inp} = C_3 \cdot \frac{P_v}{P_m - P_v} \quad (20)$$

where:

$$C_3 = C_2 \cdot \rho \cdot v_c \cdot L_v \cdot A$$

It must be noticed that $\Delta \epsilon_T$ given in the last equation is function of p_m and temperature.

Solving this equation for given operating temperature (given p_v), the optimum value of p_m can be calculated by the following expression:

$$p_{m,opt} = p_v + \sqrt{\frac{C_3 \cdot P_v}{P_{inp} \cdot K}} \quad (21)$$

for : $p_o > p_m > p_s$

Any increase or decrease of p_m from $p_{m,opt}$. would result an increase in temperature given by :

$$\Delta T = [K \cdot P_{inp} \cdot (p_m - p_v)^2 - C_3 p_v] \left[\frac{1}{p_m C_3 \left(\frac{dp_v}{dt} \right)} \right] \Delta p_{mo} \quad (22)$$

Referring to equations (7), (9) and (10) and as:

$$p_m = p_o - \Delta p_m$$

p_m is found to be function of both Q_n and H .

For given working conditions, ambient temperature and vapour pressure; if Q_n is taken to be constant, the increase of temperature may be given

* Equation (21) is calculated for the case neglecting the effect of vapour bubbles liberation ($\Delta \epsilon_v$).

as function of the variation of oil optimum initial height in the tank (H_o) as follows:

$$\Delta T = \frac{\Delta p_o^2 \cdot A_T [K \cdot P_{inp} - \frac{C_3 \cdot P_V}{(p_m - p_V)^2}] \cdot [1 - e^{-T_1/\tau} (1 + \frac{T_1}{\tau})] \cdot \Delta H_o}{Q_n \cdot p_o^n \cdot T_1 [C_3 \cdot p_m \cdot dp_V/dt + A_T U]}$$

From which the optimum height of oil may be determined by putting ($T=0$) which returns back to give $p_{m,opt.}$; hence the optimum level of oil may be also evaluated.

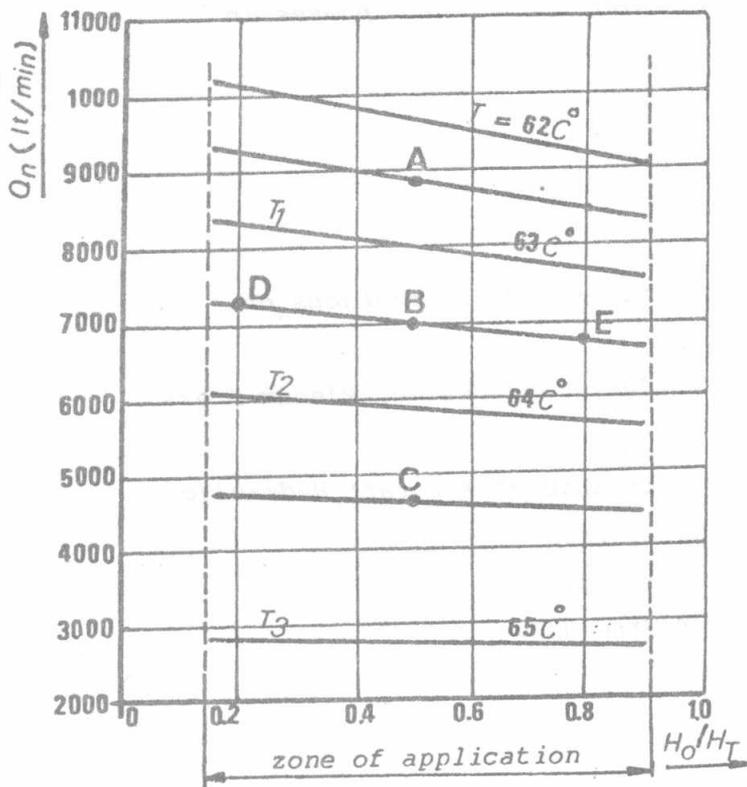


Fig. 7. Chart of calculation of the optimum height of oil in the tank.

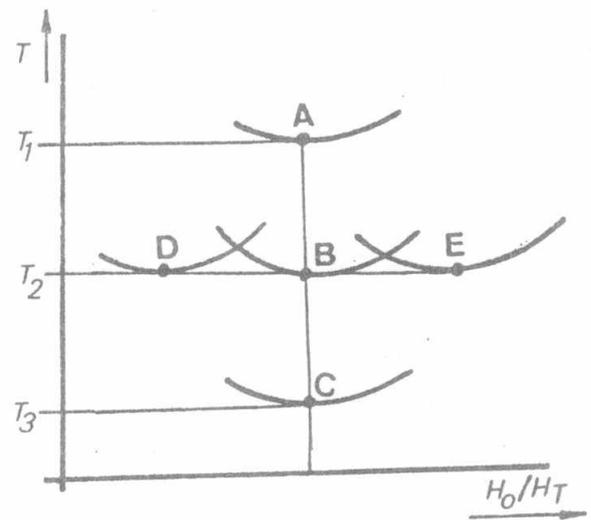


Fig. 8. Variation of temperature with other heights than optimum

Case study was developed to show that the temperature increase if oil level is changed from its optimum value as shown in figure (8).

Figure 7 shows an example of the final chart, indicating the procedure of determination of the optimum oil level height if given the temperature of working oil and the operating rate of discharge.

CONCLUSION

For certain operating conditions (working power, discharges...etc.) with certain design parameters (construction, dimensions, oil properties...etc.) an optimum level height may be evaluated. If the oil level alters from its optimum value (decreases or increases) the working oil temperature increases. This will be useful in both design and working phases in open hydraulic circuits,

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NOMENCLATURE

- A surface area of tank.
- A' area of interface of air and oil.
- A_n area of breathing nozzle.
- A_T tank cross sectional area.
- B Bulk's modulus of air (assuming polytropic process: $B=n.p$).

C_d	discharge coefficient of breather.
C_1, C_2, C_3	constants.
D	oil vapour diffusivity in the tank.
H_T	total tank height.
K_1	constants.
L_v	latent heat of vaporization of air.
n	polytropic exponent.
n_1	constant.
p	pressure inside the air chamber.
p_{cr}	air cushion critical pressure driving cavitation.
P_G	rate of heat generation.
P_{inp}	Input power.
p_m	mean absolute pressure during suction.
$p_{m,opt.}$	optimum mean pressure in the air cushion.
p_o	atmospheric pressure.
p_s	absolute steady pressure in the cushion.
p_v	saturation oil pressure at temperature T .
Q_a	air flow rate entering the tank.
Q_n	oil net flow rate leaving the tank.
Q_o & Q_i	delivery and return oil flow rate.
q_l	latent heat flux.
q_s	sensible heat flux.
T	oil temperatre.
t	time.
T_1	duration of one stroke.
U	overall heat transfer coefficient.
V_{ao}	initial volume of air cushion.
V_T	total tank volume.
v_c	mean velocity of air bulk due to convective motion.
v_s	mean velocity of air cushion bulk.
w	concentration of oil vapour per Kg of dry air.
y	supplementary displacement of oil level in the sens of increasing the air chamber volume.

$\Delta \epsilon_a$	<i>drop in air solubility.</i>
$\Delta \epsilon_T$	<i>total volumetric reduction of oil feeding the system; due to aeration and evaporation.</i>
$\Delta \epsilon_v$	<i>ratio of oil vapour volume to the total liquid volume.</i>
ΔH_o	<i>oil height deviation from the optimum.</i>
ΔP_G	<i>increase in rate of heat generation.</i>
Δp_m	<i>mean underpressure from the atmospheric, in case of suction.</i>
Δp_{mo}	<i>mean pressure deviation from its optimum value.</i>
Δp_o	<i>steady underpressure from the atmospheric; in case of suction.</i>
ΔT	<i>temperature difference.</i>
ϵ_a	<i>solubility of air in working oil.</i>
η_o	<i>overall efficiency of the system.</i>
η_v	<i>volumetric efficiency of the system; taking into consideration both aeration and cavitation.</i>
η_{vo}	<i>volumetric efficiency of the system.</i>
ρ	<i>density of air.</i>
τ	<i>time constant of the response.</i>